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APPLICATION NO.	FILING DATE	FIRST NAMED INVENTOR	ATTORNEY DOCKET NO.	CONFIRMATION NO
10/053,085	11/09/2001	Raymond J. Gorte	PENN.N2437 C	5527
23967	7590 06/17/2003			
HUNTON & WILLIAMS			EXAMINER	
1900 K STRE	UAL PROPERTY DEPART ET, N.W.	YUAN, DAH WEI D		
SUITE 1200 WASHINGTON, DC 20006-1109			ARTUNIT	PAPER NUMBER
	,		1745	
	•		DATE MAILED: 06/17/2003	

Please find below and/or attached an Office communication concerning this application or proceeding.

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-		Application No	. Applicant(s)				
		10/053,085	GORTE ET A	L. /			
	Office Action Summary	Examiner	Art Unit				
		Dah-Wei D. Yua		·			
The MAILING DATE of this communication appears on the cover sheet with the correspondence address Period for Reply							
A SHO THE M Extensi after SI - If the pr - If NO pr - Failure - Any rep	RTENED STATUTORY PERIOD IN AILING DATE OF THIS COMMUN ons of time may be available under the provision X (6) MONTHS from the mailing date of this compared for reply specified above is less than thirty (eriod for reply is specified above, the maximum so to reply within the set or extended period for reply ly received by the Office later than three months patent term adjustment. See 37 CFR 1.704(b).	IICATION. s of 37 CFR 1.136(a). In no event, how munication. (30) days, a reply within the statutory m statutory period will apply and will expir y will, by statute, cause the application	vever, may a reply be timely filed inimum of thirty (30) days will be considered to SIX (6) MONTHS from the mailing date of the to become ABANDONED (35 U.S.C. & 133)	his communication.			
1)	Responsive to communication(s) f	iled on					
2a) <u></u> □	This action is FINAL .	2b) This action is non-	inal.				
	Since this application is in condition closed in accordance with the prace of Claims			o the merits is			
4)⊠ C	claim(s) 1-53 is/are pending in the	application.					
48	a) Of the above claim(s) <u>31-53</u> is/a	are withdrawn from consider	ation.				
5)□ C	Claim(s) is/are allowed.						
6)⊠ C	claim(s) <u>1-30</u> is/are rejected.						
7) 🗌 C	claim(s) is/are objected to.						
8) C Application	claim(s) are subject to restri n Papers	iction and/or election require	ement.	-			
9) <u></u> ⊤ŀ	ne specification is objected to by the	ne Examiner.					
10)[] Th	ne drawing(s) filed on is/are	: a) ☐ accepted or b) ☐ object	ted to by the Examiner.				
	Applicant may not request that any ob-		-	• •			
	11) The proposed drawing correction filed on is: a) ☐ approved b) ☐ disapproved by the Examiner.						
	If approved, corrected drawings are re		ction.				
	ne oath or declaration is objected t	o by the Examiner.					
	der 35 U.S.C. §§ 119 and 120						
	cknowledgment is made of a claim	n for foreign priority under 3	5 U.S.C. § 119(a)-(d) or (f).				
•	All b) Some * c) None of:						
	1. Certified copies of the priority documents have been received.						
	 2. Certified copies of the priority documents have been received in Application No. 3. Copies of the certified copies of the priority documents have been received in this National Stage 						
		national Bureau (PCT Rule	17.2(a)).	nal Stage			
14)⊠ Ac	knowledgment is made of a claim	for domestic priority under	85 U.S.C. § 119(e) (to a provision	onal application).			
	The translation of the foreign la knowledgment is made of a claim						
1) Notice (2) Notice (3) Informa	of References Cited (PTO-892) of Draftsperson's Patent Drawing Review (tion Disclosure Statement(s) (PTO-1449)		Interview Summary (PTO-413) Pape Notice of Informal Patent Application Other:				
J.S. Patent and Trad PTO-326 (Rev.		Office Action Summary	Part of Paper N				

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THE USE OF SULFUR-CONTAINING FUELS FOR DIRECT OXIDATION FUEL CELLS

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Examiner: Yuan S.N. 10/053,085 Art Unit: 1745 June 6, 2003

Election/Restrictions

1. Applicant's election of Group I, claims 1-30, in Paper No. 10 is acknowledged. Because applicant did not distinctly and specifically point out the supposed errors in the restriction requirement, the election has been treated as an election without traverse (MPEP § 818.03(a)).

Claim Rejections - 35 USC § 103

- 2. The following is a quotation of 35 U.S.C. 103(a) which forms the basis for all obviousness rejections set forth in this Office action:
 - (a) A patent may not be obtained though the invention is not identically disclosed or described as set forth in section 102 of this title, if the differences between the subject matter sought to be patented and the prior art are such that the subject matter as a whole would have been obvious at the time the invention was made to a person having ordinary skill in the art to which said subject matter pertains. Patentability shall not be negatived by the manner in which the invention was made.
- 3. Claims 1-6,9-27,30 are rejected under 35 U.S.C. 103(a) as being unpatentable over Wallin (US 6,017,647) in view of Anumakonda et al. (US 6,221,280).

With respect to claim 1, Wallin teaches a solid oxide fuel cell comprising a electrolyte membrane of a ceramic oxygen ion conductor, a porous anode in contact with the electrolyte membrane on the fuel side of the cell, and a porous cathode in contact the electrolyte membrane on the oxidant side of the cell. The anode is typically a ceramic-metal composite. The net electrochemical reaction involves charge transfer steps that occur at the interface between the ionically conductive electrolyte membrane, the electronically-conductive electrode and the vapor

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phase. The vapor phase involves fuel for the anode and oxygen for the cathode. See Column 1, Lines 30-42.

However, Wallin does not disclose the characteristics of the fuel used for the aforementioned solid oxide fuel cell. Anumakonda et al. teach the use of sulfur-containing heavy hydrocarbon fuels for a solid oxide fuel cell. The hydrocarbon fuel is a liquid hydrocarbon having at least six carbon atoms and a sulfur content of at least 50 ppm. In one embodiment, the JP-8 fuel has a sulfur content of about 3000 ppm. The feed, containing the vaporized fuel and oxygen, is partially oxidized by a catalytic reaction to convert the hydrocarbon to hydrogen and carbon monoxide. As a result, the use of catalytic partial oxidation process to produce fuel enables a simplified overall system design. See Abstract, Column 1, Lines 11-15; Column 4, Lines 7-9,35-39. Therefore, it would have been obvious to one of ordinary skill in the art to use a fuel having sulfur content of at least 50 ppm to about 3000 ppm on the solid oxide fuel cell of Wallin, because Anumakonda et al. teach the processing and use of a sulfur-containing hydrocarbon fuel, such as JP-8, to simplify the overall design of a fuel cell system.

With respect to claims 2-6,9, Anumakonda et al. teach the conversion of refinery liquid hydrocarbon fuels, such as gasoline and naphtha, to hydrogen/carbon monoxide gas streams by partial oxidation process. The hydrocarbon fuels further comprises fuels, such as JP-4 jet fuel, JP-5 jet fuel, JP-8 jet fuel, No. 2 fuel oil, diesel oil, kerosene, and decane. See Column 2, Lines 6-18; Column 5, Lines 39-43; column 13, Lines 15-28. Therefore, it would have been obvious to

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one of ordinary skill in the art to use fuel, including jet fuel, gasoline, naphtha, fuel oil, diesel oil, kerosene, and decane, on the solid oxide fuel cell of Wallin, because Anumakonda et al. teach the processing and use of a sulfur-containing hydrocarbon fuel can simplify the overall design of a fuel cell system.

With respect to claims 10-14, Anumakonda et al. teach the military specification for maximum sulfur content in logistic fuels, such as Jet A, JP-4, JP-5, and JP-8, is 0.3 wt% (3000 ppm). Typically, however, commercially available jet fuels have a total sulfur content of about 0.05-0.07 wt.% (500-700 ppm). See Column 2, Lines 38-44. Therefore, it would have been obvious to one of ordinary skill in the art to use a fuel having sulfur content of at about 500 to about 700 ppm on the solid oxide fuel cell of Wallin, because Anumakonda et al. teach the processing and use of a sulfur-containing hydrocarbon fuel, such as JP-4, JP-5, and JP-8, can simplify the overall design of a fuel cell system.

With respect to claim 15, Wallin discloses the electrolyte membrane is a ceramic oxygen ion conductor. See Column 1, Lines 30-32.

With respect to claims 16-19, Wallin teaches suitable ionically conductive materials include doped zirconia such as yttria-stabilized zirconia, scandium-doped zirconia, gadolinium-doped ceria, and rare earth or alkaline earth-doped LaAGaO₃. See Column 4, lines 49-59.

With respect to claim 20, Wallin teaches process to generate electrical energy by using a solid oxide fuel cell, which comprises a electrolyte membrane of a ceramic oxygen ion conductor, a porous anode in contact with the electrolyte membrane on the fuel side of the cell,

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and a porous cathode in contact the electrolyte membrane on the oxidant side of the cell. The anode is typically a ceramic-metal composite. The net electrochemical reaction involves charge transfer steps that occur at the interface between the ionically conductive electrolyte membrane, the electronically-conductive electrode and the vapor phase. The vapor phase involves fuel for the anode and oxygen for the cathode. See Column 1, Lines 30-42.

However, Wallin does not disclose the characteristics of the fuel used for the aforementioned solid oxide fuel cell. Anumakonda et al. teach the use of sulfur-containing heavy hydrocarbon fuels for a solid oxide fuel cell. The hydrocarbon fuel is a liquid hydrocarbon having at least six carbon atoms and a sulfur content of at least 50 ppm. In one embodiment, the JP-8 fuel has a sulfur content of about 3000 ppm. The feed, containing the vaporized fuel and oxygen, is partially oxidized by a catalytic reaction to convert the hydrocarbon to hydrogen and carbon monoxide. As a result, the use of catalytic partial oxidation process to produce fuel enables a simplified overall system design. See Abstract, Column 1, Lines 11-15; Column 4, Lines 7-9,35-39. Therefore, it would have been obvious to one of ordinary skill in the art to use a fuel having sulfur content of at least 50 ppm to about 3000 ppm on the process of Wallin, because Anumakonda et al. teach the processing and use of a sulfur-containing hydrocarbon fuel, such as JP-8, can simplify the overall design of a fuel cell system.

With respect to claims 21-27, Anumakonda et al. teach the conversion of refinery liquid hydrocarbon fuels, such as gasoline and naphtha, to hydrogen/carbon monoxide gas streams by partial oxidation process. The hydrocarbon fuels further comprises fuels, such as JP-4 jet fuel,

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JP-5 jet fuel, JP-8 jet fuel, No. 2 fuel oil, diesel oil, kerosene and decane. See Column 2, Lines 6-18; Column 9, Lines 1-4; column 13, Lines 15-28. Therefore, it would have been obvious to one of ordinary skill in the art to use fuel, including jet fuel, gasoline, naphtha, fuel oil, diesel oil, kerosene and decane, on the process of Wallin, because Anumakonda et al. teach the processing and use of a sulfur-containing hydrocarbon fuel can simplify the overall design of a fuel cell system.

With respect to claim 30, Anumakonda et al. teach the military specification for maximum sulfur content in logistic fuels, such as Jet A, JP-4, JP-5, and JP-8, is 0.3 wt% (3000 ppm). Typically, however, commercially available jet fuels have a total sulfur content of about 0.05-0.07 wt.% (500-700 ppm). See Column 2, Lines 38-44. Therefore, it would have been obvious to one of ordinary skill in the art to use a fuel having sulfur content of at about 500 to about 700 ppm on the process of Wallin, because Anumakonda et al. teach the processing and use of a sulfur-containing hydrocarbon fuel, such as JP-4, JP-5, and JP-8, can simplify the overall design of a fuel cell system.

4. Claims 1,2,7,8,20,28,29 are rejected under 35 U.S.C. 103(a) as being unpatentable over Wallin (US 6,017,647) in view of Fasano et al. (US 6,051,330) as evidenced by Yamauchi et al. (US 4,228,033).

With respect to claims 1,2,7,8, Wallin teaches a solid oxide fuel cell comprising a electrolyte membrane of a ceramic oxygen ion conductor, a porous anode in contact with the electrolyte membrane on the fuel side of the cell, and a porous cathode in contact the electrolyte

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membrane on the oxidant side of the cell. The anode is typically a ceramic-metal composite.

The net electrochemical reaction involves charge transfer steps that occur at the interface between the ionically conductive electrolyte membrane, the electronically-conductive electrode and the vapor phase. The vapor phase involves fuel for the anode and oxygen for the cathode.

See Column 1, Lines 30-42. However, Wallin does not disclose the characteristics of the fuel used for the aforementioned solid oxide fuel cell. Fasano et al. teach the use of light hydrocarbons, such as methane, propane, ethanol and methanol, as fuel for a solid oxide fuel cell because they produce less carbonaceous material build-up in the anode. See Column 1, Lines 5-8, 61 to Column 2, Line 2. The typical sulfur content in the methanol is found to be between 1 to 5 ppm as documented in Yamauchi et al. See Column 45, Line 34; Column 58, Line 54.

Therefore, it would have been obvious to one of ordinary skill in the art to use a light hydrocarbon fuel, such as methanol having sulfur content of 1 to 5 ppm, on the solid oxide fuel cell of Wallin, because Fasano et al. teach the use of a light hydrocarbon fuel can reduce the build-up of carbonaceous material in the anode of a solid oxide fuel cell.

With respect to claim 20, Wallin teaches process to generate electrical energy by using a solid oxide fuel cell, which comprises a electrolyte membrane of a ceramic oxygen ion conductor, a porous anode in contact with the electrolyte membrane on the fuel side of the cell, and a porous cathode in contact the electrolyte membrane on the oxidant side of the cell. The anode is typically a ceramic-metal composite. The net electrochemical reaction involves charge transfer steps that occur at the interface between the ionically conductive electrolyte membrane,

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the electronically-conductive electrode and the vapor phase. The vapor phase involves fuel for the anode and oxygen for the cathode. See Column 1, Lines 30-42.

However, Wallin does not disclose the characteristics of the fuel used for the aforementioned solid oxide fuel cell. Fasano et al. teach the use of light hydrocarbons, such as methane, propane, ethanol and methanol, as fuel for a solid oxide fuel cell because they produce less carbonaceous material build-up in the anode. See Column 1, Lines 5-8, 61 to Column 2, Line 2. The typical sulfur content in the methanol is found to be between 1 to 5 ppm as documented in Yamauchi et al. See Column 45, Line 34; Column 58, Line 54. Therefore, it would have been obvious to one of ordinary skill in the art to use a light hydrocarbon fuel, such as methanol having a sulfur content of 1 to 5 ppm, on the process of Wallin, because Fasano et al. teach the use of a light hydrocarbon fuel can reduce the build-up of carbonaceous material in the anode of a solid oxide fuel cell.

Any inquiry concerning this communication or earlier communications from the examiner should be directed to Dah-Wei D. Yuan whose telephone number is (703) 308-0766. The examiner can normally be reached on Monday-Friday (8:00-5:00).

If attempts to reach the examiner by telephone are unsuccessful, the examiner's supervisor, Patrick J. Ryan, can be reached on (703) 308-2383. The fax phone numbers for the organization where this application or proceeding is assigned are (703) 872-9310 for regular communications and (703) 872-9311 for After Final communications.

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Any inquiry of a general nature or relating to the status of this application or proceeding should be directed to the receptionist whose telephone number is (703) 308-0661.

Delive y

Dah-Wei D. Yuan

June 6, 2003